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(19) (CA) **APPLICATION FOR CANADIAN PATENT** (12)

(54) **Process for Bleaching of Lignocellulose-Containing Pulp**

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Notice: This application is as filed and may therefore contain an incomplete specification.



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Abstract

The present invention relates to a process for delignification and bleaching of chemically digested lignocellulose-containing pulp, wherein the pulp is acid treated at a pH of between about 1 and about 6, whereupon a water-soluble mixture of a magnesium compound and a calcium compound is added at a pH of between about 1 and about 7 before the pulp is treated with a chlorine-free bleaching agent. The chlorine-free bleaching agent includes hydrogen peroxide. After the treatment according to the invention, the pulp may be finally bleached to the desired brightness, suitably with a chlorine-free bleaching agent, such as ozone, to completely avoid formation and discharge of AOX.

1 This invention relates to a process for bleaching of
lignocellulose-containing pulp.

This application is a division of Canadian Patent
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5 The present invention relates to a process for delig-
nification and bleaching of chemically digested lignocellulo-
se-containing pulp, wherein the pulp is acid treated at a pH
of between about 1 and about 6, whereupon a water-soluble
mixture of a magnesium compound and a calcium compound is
10 added at a pH of between about 1 and about 7 before the pulp
is treated with a chlorine-free bleaching agent comprising
hydrogen peroxide at a pH of from about 8 up to about 12. The
initial acidic treatment removes the trace metals of the pulp,
whereas the subsequent addition of alkaline earth metal ions
15 in aqueous solution returns the ions to the positions in the
pulp where they have a particularly beneficial effect on the
preservation of the cellulose chains and, consequently, on the
viscosity, as well as on the consumption of bleaching agent in
the subsequent bleaching step. After the treatment according
20 to the invention, the pulp may be finally bleached to the
desired brightness, suitably with a chlorine-free bleaching
agent, such as ozone, to completely avoid formation and
discharge of AOX.

Background

25 In the production of chemical pulp of high brightness,
wood chips are first cooked to separate the cellulose fibres.
Part of the lignin holding the fibres together is thus
degraded and modified, such that it can be removed by subse-
quent washing. However, in order to obtain sufficient bright-
30 ness, more lignin has to be removed, together with brightness-
impairing (chromophoric) groups. This is frequently effected
by delignification with oxygen, followed by bleaching in
several stages.

For environmental reasons, it has become increasingly
35 common to treat chemical pulp with chlorine-free bleaching
agents already in the first bleaching steps. The big advantage
is the drastic reduction in the discharges of chlorinated
organic substances detrimental to the environment, owing to
the combined effect of a smaller amount of chlorine-containing
40 bleaching agents and lower content of lignin, which is the
organic substance primarily reacting with the chlorine.

It is known to use chlorine-free bleaching agents, such

as hydrogen peroxide, peracetic acid or ozone, already in the prebleaching. However, the delignification and consumption of the bleaching agent become less effective than with chlorine-containing bleaching agents, unless the pulp is pretreated.

5 Thus, a hydrogen peroxide treatment in an alkaline environment is disturbed by the presence in the pulp of ions of certain metals, such as Mn, Cu and Fe. These metal ions cause degradation of hydrogen peroxide, thereby reducing the efficiency of the peroxide treatment and increasing the consumption of
10 peroxide. According to CA 1,206,704, this can be counteracted by pretreating the pulp with an acid, such as sulphuric acid or nitric acid, whereby the concentration of all types of metal ions is reduced. However, by this treatment also metal ions, for example Mg, which are advantageous to the peroxide
15 treatment disappear, which ions stabilize the peroxide and increase the selectivity of the peroxide.

CA 575,636 discloses the addition of magnesium sulphate to stabilize alkaline peroxide solutions. However, the addition is made directly to the bleaching liquor and in
20 alkaline environment insoluble magnesium hydroxide precipitates. Furthermore, US 4,222,819 discloses the addition of magnesium ions to acidic peroxide solutions, but also in this case the addition is made directly to the bleaching liquor. None of the related methods makes possible diffusion of the
25 magnesium ions into the pulp to such an extent, that a pulp of high brightness and strength can be obtained.

The invention

The invention provides a process in which lignocellulose-containing pulp is treated under the conditions disclosed in
30 the claims, whereby the metal ions harmful to the subsequent bleaching are effectively removed and the profile of alkaline earth metals is restored before the pulp is bleached in a chlorine-free bleaching step.

The invention relates to a process for bleaching of
35 chemically digested lignocellulose-containing pulp, wherein the pulp is acid treated at a pH in the range from about 1 up to about 6, whereupon a mixture containing a magnesium compound and a calcium compound is added at a pH in the range from about 1 up to about 7 and in an amount of from about 0.01

kg, suitably 0.5 kg, up to about 10 kg/ton of dry pulp, calculated as magnesium and calcium, and that the pulp subsequently is treated with a chlorine-free bleaching agent comprising hydrogen peroxide at a pH of from about 8 up to about 12.

Acid treatment is an effective process to eliminate metal ions from lignocellulose-containing pulps. At the same time it is known, that ions of magnesium and calcium, especially when in their original positions in the pulp, have a positive influence on the selectivity of the delignification as well as on the stability and consumption of chlorine-free bleaching agents, such as peroxides, ozone and oxygen. The present process presents an economic solution to the problem of creating a suitable trace-metal profile for the subsequent chlorine-free bleaching, in that non-desirable metal ions are eliminated while supplied ions of magnesium and calcium essentially recover the positions in the vicinity of the cellulose chains previously occupied by ions of alkaline earth metals. This is achieved by adding a mixture of a magnesium compound and a calcium compound at such a pH and such a temperature that the compound is dissolved in water, thus enabling the diffusion required to obtain the intended effect. Furthermore, an advantage of the present process is that the pH adjustment between the treatment with acid and addition of alkaline earth metal ions becomes very limited or may be left out altogether, which is advantageous to process technique and economy.

Chlorine-free bleaching agents include inorganic peroxide compounds, such as hydrogen peroxide and sodium peroxide, organic peroxide compounds, such as peracetic acid, as well as ozone, oxygen and sodium dithionite. Suitably, hydrogen peroxide (P), oxygen (O) and ozone (Z) are used in an optional sequence or mixture. Preferably, use is made of hydrogen peroxide or mixtures of hydrogen peroxide and oxygen (PO). The sequence P-Z or (PO)-Z are especially preferred.

In the treatment with a chlorine-free bleaching agent in an alkaline environment, pH is suitably adjusted by adding to the pulp an alkali or an alkali-containing liquid, such as sodium carbonate, sodium hydrogen carbonate, sodium hydroxide,

oxidized white liquor or magnesium hydroxide slurry. Suitably, the magnesium hydroxide slurry is taken from the chemical handling system in the production of sulphite pulp with magnesium as base, i.e. magnesite pulp.

5 The acid treatment suitably is carried out with an acid. The acids used are inorganic acids, suitably sulphuric acid, nitric acid, hydrochloric acid or residual acid from a chlorine dioxide reactor, either separately or in an optional mixture. Preferably, sulphuric acid is employed.

10 Use is suitably made of magnesium-containing compounds, such as magnesium sulphate or magnesium chloride, and calcium-containing compounds, such as calcium chloride or calcium oxide. The combination of temperature and pH at the addition of the mixture of a magnesium compound and a calcium compound
15 is always so chosen that the compound is in aqueous solution when contacted with the pulp.

In the process according to the invention, the acid treatment is carried out at a pH of from about 1 up to about 6, suitably from 1.5 up to 5, preferably from 2 up to 4. It is
20 especially preferred that the acid treatment is carried out at a pH of from 2 up to 3. When magnesium is the alkaline earth metal in the compound containing an alkaline earth metal, the addition is made at a pH in the range from about 1 up to about 7, suitably in the range from 2 up to 6, preferably in the
25 range from 2 up to 4. It is especially preferred that the addition of magnesium is made at a pH of from 2 up to 3. When the chlorine-free bleaching agent is hydrogen peroxide, the pulp is treated at a pH of from about 8 up to about 12, preferably at a pH of from 10 up to 12. Treatment with the
30 other chlorine-free bleaching agents mentioned above, is carried out within the normal pH ranges for each bleaching agent, which are well-known to the person skilled in the art.

The treatment according to the invention is preferably carried out with a washing step between the acid treatment and
35 addition of alkaline earth metal ions, such that the trace metals that are harmful to the treatment with a chlorine-free bleaching agent are removed from the pulp suspension.

The realization of the acid treatment, a mixture of a magnesium compound and a calcium compound and a chlorine-free

bleaching agent, can be carried out at an optional position in the bleaching sequence, e.g. immediately after digestion of the pulp or after an oxygen step. The process according to the invention is preferably applied to pulp that has been delignified in an oxygen step prior to the treatment.

It is also within the scope of the invention, that the pulp in the acid treatment also can be subjected to bleaching and/or delignifying treatment. Bleaching and/or delignifying chemicals active within the pH range suitable in the acid treatment, are e.g. chlorine dioxide, ozone, peracetic acid and/or an acid peroxide-containing compound. Suitably, a combination of acid treatment and bleaching and/or delignifying treatment takes place in an ozone step.

Lignocellulose-containing pulps relate to chemical pulps of softwood and/or hardwood digested according to the sulphite, sulphate, soda or organosolv process, or modifications and/or combinations thereof. Use is suitably made of softwood and/or hardwood digested according to the sulphate process, preferably sulphate pulp of hardwood.

The treatment according to the invention can be applied to lignocellulose-containing pulps having an initial kappa number within the range from about 5 up to about 40, suitably 7 up to 32, preferably from 10 up to 20. Here, the kappa number is determined according to the standard method SCAN-C 1:77.

In the process according to the invention, the acid treatment is carried out at a temperature of from about 10 up to about 95°C, suitably from 20 up to 80°C and preferably from 40 up to 80°C, and for a period of time of from about 1 up to about 120 min, suitably from 10 up to 120 min and preferably from 20 up to 40 min. The mixture of a magnesium compound and a calcium compound is added at a temperature of from about 10 up to about 95°C, preferably from 40 up to 80°C, and for a period of time of from about 1 up to about 180 min, preferably from 20 up to 180 min and preferably from 30 up to 120 min. When the chlorine-free bleaching agent is hydrogen peroxide, the pulp is treated at a temperature of from about 30 up to about 100°C, preferably from 60 up to 90°C, and for a period of time of from about 30 up to about 300 min, suitably from 60

up to 240 min. In the acid treatment and in the addition of a mixture of magnesium and calcium ions, the pulp concentration may be from about 3 up to about 35% by weight, preferably from 3 up to 15% by weight. When the chlorine-free bleaching agent is hydrogen peroxide, the pulp concentration may be from about 3 up to about 50% by weight, suitably from 3 up to 35% by weight and preferably from 10 up to 25% by weight. Treatment with the other chlorine-free bleaching agents mentioned above, is carried out within the normal ranges of temperature, time and pulp concentration for each bleaching agent, which are well-known to the person skilled in the art.

The amount of mixture containing a magnesium compound and a calcium compound charged, lies in the range from about 0.01 up to about 10 kg/ton of dry pulp, suitably in the range from 0.5 up to 5 kg/ton of dry pulp, and preferably in the range from 2 up to 4 kg/ton of dry pulp, calculated as magnesium and calcium.

In preferred embodiments employing hydrogen peroxide as the chlorine-free bleaching agent, the amount of hydrogen peroxide, lies in the range from about 2 up to about 50 kg/ton of dry pulp, calculated as 100% hydrogen peroxide. The upper limit is not critical, but has been set for reasons of economy. The amount of hydrogen peroxide suitably lies in the range from 3 up to 30 kg/ton of dry pulp and preferably from 4 up to 20 kg/ton of dry pulp, calculated as 100% hydrogen peroxide.

After the acid treatment, a mixture of a magnesium compound and a calcium compound, and a chlorine-free bleaching agent, the pulp can be used for direct production of paper with a lower demand of brightness. Alternatively, the pulp may be finally bleached to the desired higher brightness, by treatment in one or more steps. Suitably, the final bleaching is also carried out with chlorine-free bleaching agents of the type mentioned above, optionally with intermediate alkaline extraction steps, which may be reinforced with peroxide and/or oxygen. In this way, the formation and discharge of AOX is completely eliminated. Suitably, the final bleaching is carried out with ozone in one or more steps. By the treatment according to the invention, the lignin content has been

reduced to a sufficiently low level before any chlorine-containing bleaching agents are used. Therefore, chlorine dioxide and/or hypochlorite may well be used in one or more final bleaching steps without causing formation of large amounts of AOX.

Moreover, use of the process according to the invention means that the brightness and kappa number of the resulting pulp is higher and lower, respectively, than with the processes in which a mixture of a magnesium compound and a calcium compound is not added at all or is added at a higher pH. In a process for bleaching chemical pulps, the aim is a high brightness as well as a low kappa number, the latter meaning a low content of undissolved lignin. At the same time, the consumption of the chlorine-free bleaching agent should be as low as possible meaning lower treatment costs. In the process according to the invention, these objects are met, as is apparent from the Examples. Furthermore, the strength of the pulp, measured as viscosity, is sufficient, which means that the pulp contains cellulose chains which are long enough to give a strong product.

The invention and its advantages are illustrated in more detail by the Examples below which, however, are only intended to illustrate the invention and are not intended to limit the same. The percentages and parts stated in the description, claims and examples, refer to percent by weight and parts by weight, respectively, unless anything else is stated.

Example 1

Sulphate pulp of softwood having a kappa number of 17, a brightness of 35% ISO and a viscosity of 970 dm³/kg was treated with sulphuric acid at a pH of 2.0. The pulp was treated at a temperature of 60°C for 30 min, the pulp concentration being 10% by weight. After washing the pulp with water, magnesium was added in the form of an aqueous solution containing MgSO₄, to give a concentration of magnesium in the pulp of at least 500 ppm. In the tests, the pH at the time of the addition was varied between 2.3 and 11.5 by addition of sulphuric acid. Then, the pulp was bleached with hydrogen peroxide at a temperature of 90°C, the residence time and pulp concentration being 180 min and 15% by weight, respectively.

The final pH was 11.5, and the addition of hydrogen peroxide was 15 kg/ton of dry pulp, calculated as 100% hydrogen peroxide. For comparative purposes, magnesium was added directly to the hydrogen peroxide step under the conditions stated above, in accordance with the prior art. To provide a further comparison, the pulp was also treated with only sulphuric acid and hydrogen peroxide under the conditions stated above. The kappa number, viscosity and brightness of the pulp were determined according to SCAN Standard Methods, and the consumption of hydrogen peroxide was determined by iodometric titration. The test results appear from the Table below.

TABLE I

pH at the addition of Mg	Kappa number step 2	Viscosity step 2 (dm ³ /kg)	Brightness step 2 (% ISO)	Residual H ₂ O step 2 (kg/ton)
2.3	9.1	903	61.0	1.5
4.7	9.2	910	60.0	1.0
9.5	9.8	930	56.1	0.9
11.5	10.0	940	52.2	0.2
---- *	9.8	890	54.1	0.5
2.3 **	9.9	875	48.2	0.0

* Magnesium added directly to the alkaline hydrogen peroxide step.

** No magnesium added.

As is apparent from the Table, the treatment according to the present invention with MgSO₄ at a pH in the range from about 2 up to about 6 is essential to give maximum increase in brightness and maximum reduction of the kappa number, as well as minimum decrease in viscosity and minimum consumption of hydrogen peroxide. Furthermore, the importance of the magnesium ions for the increase in brightness appears from the comparison at a pH of 2.3, where, in the final test, the peroxide treatment was preceded only by acidic treatment.

Example 2

Oxygen-delignified sulphate pulp of softwood having a kappa number of 13.7, a brightness of 37.1% ISO and a viscosity of 1057 dm³/kg, was treated in a first step with

15 kg of sulphuric acid/ton of dry pulp at a pH of 1.9. The pulp was treated at a temperature of 50°C for 60 min, the pulp concentration being 10% by weight. After washing the pulp with water, in a second step between 0.1 and 1.5 kg of magnesium/ton of dry pulp was added in the form of an aqueous solution containing $MgSO_4$. Magnesium was added at a pH of 4.1, a temperature of 50°C for 60 min and with a pulp concentration of 3.5% by weight. Then, the pulp was bleached with hydrogen peroxide at a temperature of 90°C, the residence time and pulp concentration being 240 min and 10% by weight, respectively. The final pH was 11.5 and the addition of hydrogen peroxide was 20 kg/ton of dry pulp calculated as 100% hydrogen peroxide. For comparative purposes, the pulp was also treated with only sulphuric acid and hydrogen peroxide under the conditions stated above. The kappa number, viscosity and brightness were determined according to SCAN Standard Methods. The results after bleaching with hydrogen peroxide appear from the Table below.

TABLE II

Amount of Mg added in step 2 (kg/ton)	Amount of Mg in pulp after step 2 (ppm)	Kappa no. step 3	Viscosity step 3 (dm^3/kg)	Brightness step 3 (% ISO)
0	3,7	9.6	900	51.5
0.1	130	8.2	870	61.8
0.3	250	7.8	864	65.1
0.75	370	7.7	855	65.9
1.5	480	7.6	845	67.3

As is apparent from the Table, acid treatment followed by addition of dissolved magnesium and bleaching with hydrogen peroxide according to the present invention, positively influence the pulp as regards kappa number, viscosity and brightness.

Example 3

The oxygen-delignified sulphate pulp of softwood used in Example 2, was treated in the sequences D - EOP - Z - P (test 1) and D - EOP - Z - Mg - P (test 2), where the conditions in each step were equal in both sequences.

D and EOP relate to a conventional chlorine dioxide step and a conventional alkaline extraction step reinforced with hydrogen peroxide and oxygen, respectively. Z relates to an ozone step with a pH of 2.3. Mg relates to the addition of 1 kg of magnesium/ton of dry pulp, in the form of an aqueous solution containing $MgSO_4$. Magnesium was added at a pH of 4.1, a temperature of 50°C for 30 min, the pulp concentration being about 3% by weight. P relates to a hydrogen peroxide step, where the pulp was treated at a temperature of 80°C for 120 min. The final pH was about 11.5 and the addition of hydrogen peroxide was 5 kg/ton of dry pulp calculated as 100% hydrogen peroxide. The viscosity and brightness were determined according to SCAN Standard Methods. The results after bleaching with hydrogen peroxide appear from the Table below.

TABLE III

Test	Amount of Mg added (kg/ton)	Amount of Mg in pulp after addition (ppm)	Viscosity (dm^3/kg)	Brightness (% ISO)
1	0	16	820	86.3
2	1.0	255	872	88.4

As is apparent from the Table, addition of dissolved magnesium after an initial acid treatment with ozone and bleaching with hydrogen peroxide according to the present invention, positively influence the pulp as regards viscosity and brightness.

Example 4

The oxygen-delignified sulphate pulp of softwood used in Example 2, was treated in the sequences Step1 - P_1 - Z - P_2 (test 1) and Step1 - P_1 - Z - Mg - P_2 (test 2), where the conditions in each step were equal in both sequences. Step1 relates to treatment with EDTA at a pH of 5. Z relates to an ozone step with a pH of 2.3, the pulp concentration being 10% by weight. Mg relates to the addition of 1 kg of magnesium/ton of dry pulp, in the form of an aqueous solution containing $MgSO_4$. Magnesium was added at a pH of 4.1, a temperature of 50°C for 30

min, the pulp concentration being about 3% by weight. P_2 relates to a hydrogen peroxide step, where the pulp was treated at a temperature of 80°C for 120 min. The final pH was about 11.5 and the addition of hydrogen peroxide was 5 kg/ton of dry pulp calculated as 100% hydrogen peroxide. For comparative purposes, the pulp was also treated in the sequence Step1 - P_1 - Z - (PMg) (test 3). (PMg) relates to the addition of magnesium in the second alkaline hydrogen peroxide step under the conditions stated above, in accordance with the prior art. The viscosity and brightness were determined according to SCAN Standard Methods, and the consumption of hydrogen peroxide was determined by iodometric titration. The results after the second hydrogen peroxide step appear from the Table below.

TABLE IV

Test	Amount of Mg added (kg/ton)	Amount of Mg in pulp (ppm)	Viscosity (dm ³ /kg)	Bright- ness (% ISO)	H ₂ O ₂ con- sumed in P_2 (% of added)
1	0	9	794	80.9	76
2	1.0	300	856	83.9	28
3	1.0	120	809	81.6	60

As is apparent from the Table, addition of magnesium within the present pH range before bleaching with hydrogen peroxide, positively influence the pulp as regards viscosity and brightness and reduces the consumption of hydrogen peroxide.

Example 5

Sulphate pulp of softwood having a kappa number of 10, a brightness of 42.5 % ISO and a viscosity of 986 dm³/kg was treated with 15 kg/ton sulphuric acid at a temperature of 50°C for 30 min and the pulp concentration being 10% by weight. pH was 5-5.5. After washing the pulp with water, magnesium, calcium or a mixture of them, was added. 1 kg/ton magnesium respectively 1.5 kg/ton calcium was added, or the total amount of the chemicals when a mixture is added. pH at the time of the addition was between 5 and 5.5, at a temperature of 60°C for 60 min. Then, the pulp was bleached with hydrogen peroxide at a

temperature of 90°C, the residence time and pulp concentration being 240 min and 15% by weight, respectively. pH was 10.5-11 and the addition of hydrogen peroxide was 35 kg/ton of dry pulp, calculated as 100% hydrogen peroxide. The kappa number and brightness of the pulp were determined according to SCAN Standard Methods, and the consumption of hydrogen peroxide was determined by iodometric titration. The test results appear from the Table below.

TABLE V

Sequence	Brightness	Kappa No.	Residual H ₂ O ₂
	%ISO		kg/t
A-Ca-P	70,5	4,58	0,15
A-Mg-P	77,5	4,44	7,3
A- (Mg+Ca) -P	81,3	4,02	8,7

The embodiments of the invention in which an exclusive property or privilege is claimed are defined as follows:

1. A process for delignification and bleaching of chemically digested lignocellulose-containing pulp, characterized in that the pulp is acid treated at a pH in the range from about 1 up to about 6, whereupon a water-soluble mixture of a magnesium compound and a calcium compound is added at a pH in the range from about 1 up to about 7 and in an amount of from about 0.01 up to about 10 kg/ton of dry pulp, calculated as magnesium and calcium, and that subsequently the pulp is delignified and bleached with a chlorine-free bleaching agent comprising hydrogen peroxide at a pH of from about 8 up to about 12.

2. A process according to claim 1, characterized in that the pulp is delignified and bleached with hydrogen peroxide at a pH of from 10 up to 12.

3. A process according to claim 1, characterized in that the chemically digested pulp is a sulphate pulp.

4. A process according to claim 1, characterized in that the water-soluble mixture of a magnesium compound and a calcium compound is added at a pH of from 2 up to 6.

5. A process according to claim 1, characterized in that the calcium compound is calcium chloride or calcium oxide.

6. A process according to claim 1 or 5, characterized in that magnesium compound is magnesium sulphate or magnesium chloride.

7. A process according to claim 1, characterized in that the pulp is washed after the acid treatment.

8. A process according to claim 1, characterized in that the chlorine-free bleaching agent consists of oxygen and hydrogen peroxide.

9. A process according to claim 8, characterized in that the pulp, after the treatment, is finally bleached with ozone in one or more steps.

10. A process according to claim 1, 2, 3, 4, 5, 7, 8 or 9, characterized in that the acid treatment is carried out at a temperature of from about 10 up to about 95°C for about 1 up to about 120 min., that the mixture of the magnesium compound and a calcium compound is added at a temperature of from about 10 up to about 95°C for about 1 up to about 180 min. and in an amount of from 0.5 up to 5 kg/ton of dry pulp, calculated as magnesium compound and calcium compound, the treated pulp having a concentration of from about 3 up to about 35% by weight, and that the pulp is bleached and delignified with hydrogen peroxide at a pH of from about 8 up to about 12.

11. A process according to claim 6, characterized in that the acid treatment is carried out at a temperature of from about 10 up to about 95°C for about 1 up to about 120 min., that the mixture of the magnesium compound and a calcium compound is added at a temperature of from about 10 up to about 95°C for about 1 up to about 180 min. and in an amount of from 0.5 up to 5 kg/ton of dry pulp, calculated as magnesium compound and calcium compound, the treated

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pulp having a concentration of from about 3 up to about 35% by weight, and that the pulp is bleached and delignified with hydrogen peroxide at a pH of from about 8 up to about 12.